



University of Brighton



Advanced Engineering Centre, University of Brighton  
**Research Seminar**

# Aerosols: environmental, technological and health science applications

**S.K. Zaripov**

**Kazan Federal University, Kazan, Russia**

# Definition

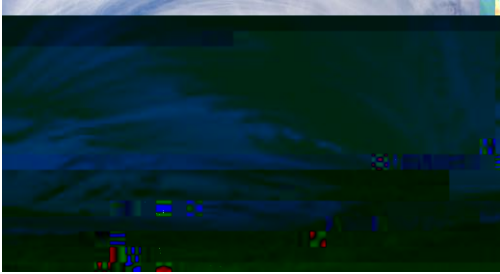
**Aerosol** is a suspension of solid or liquid particles in a gas.

Examples: dust, clouds

Bioaerosols: aerosols of biological nature (viruses, bacteria, fungi, spores, pollens)

# Aerosol sources

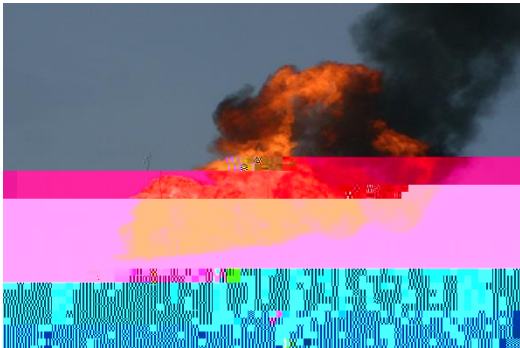
Nature aerosols



clouds



Smoke from forest fires  
Sheremetyevo 2010 08 07

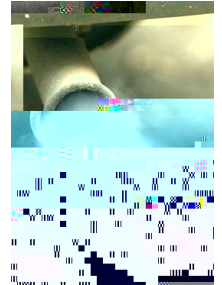


industrial fire

Sea aerosols



Dust-storm-Texas-1935



car emissions



tobacco smoke



sneeze particles

## Aerosol particle sizes

The range of diameters of aerosol particles is  $10^{-8}$  -  $10^{-4}$  m = T f 1 0 0 1 440.54 45.7 T m

# Aerosol problems

Monitoring

Health related problems

Air cleaning air filtration

Aerosol technology

## **Course aerosols**

Inertia

Gravity

## **Ultrafine particles**

Diffusion

Phoretic forces (thermophoresis, diffusiophoresis, photophoresis)

Electrostatic forces

# Human inhalability - aerosol influence

**Environment**

**Workplace**

**< 100  $\mu\text{m}$**

**inhalable**

**PM10**

**thoracic**

**< 10  $\mu\text{m}$**

**respirable**

**PM2.5**

**PM1**

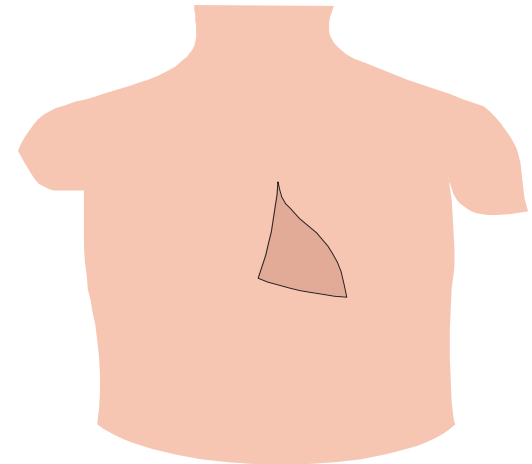
**< 5  $\mu\text{m}$**

**PM0.1**

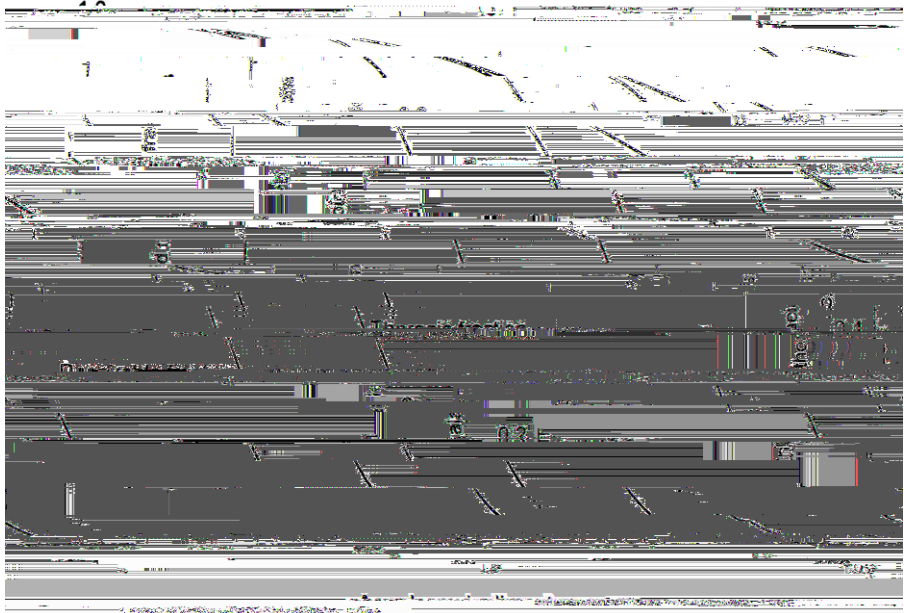
**Ultrafine**

**Nanoparticles**

**Nanoparticles**



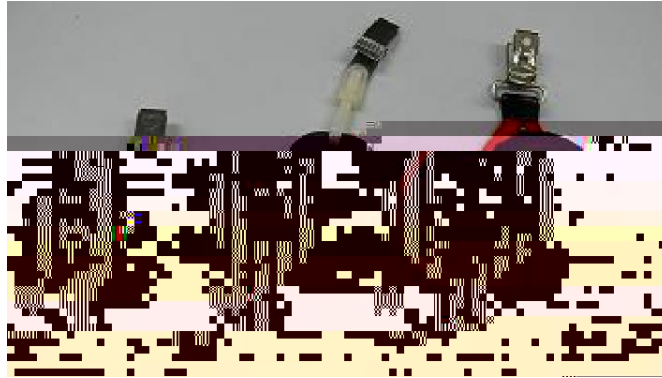
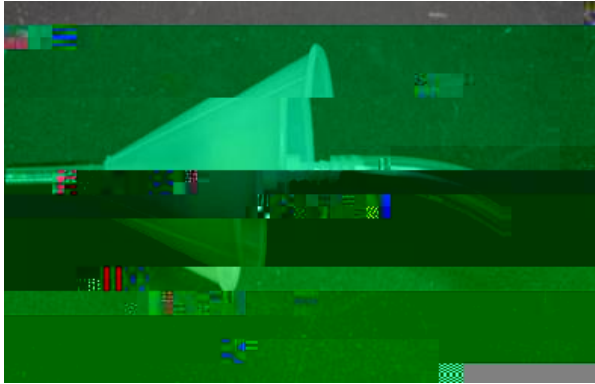
**From the lecture of Prof. W.Koch, Fraunhofer ITEM, June, 2014, Kazan**



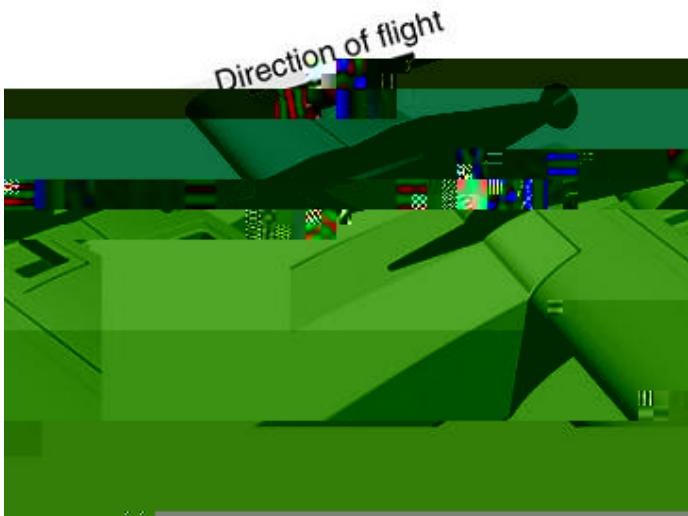
Curves of inhalable, thoracic and respirable dust fractions

# Aerosol monitoring – aerosol sampling

## Various sampler inlets



Darrah K. Schmees , Yi-Hsuan Wu and James H. Vincent



**Respicon**

## Aspiration efficiency

$$A = \frac{C_i}{C_0}$$

$C_i$

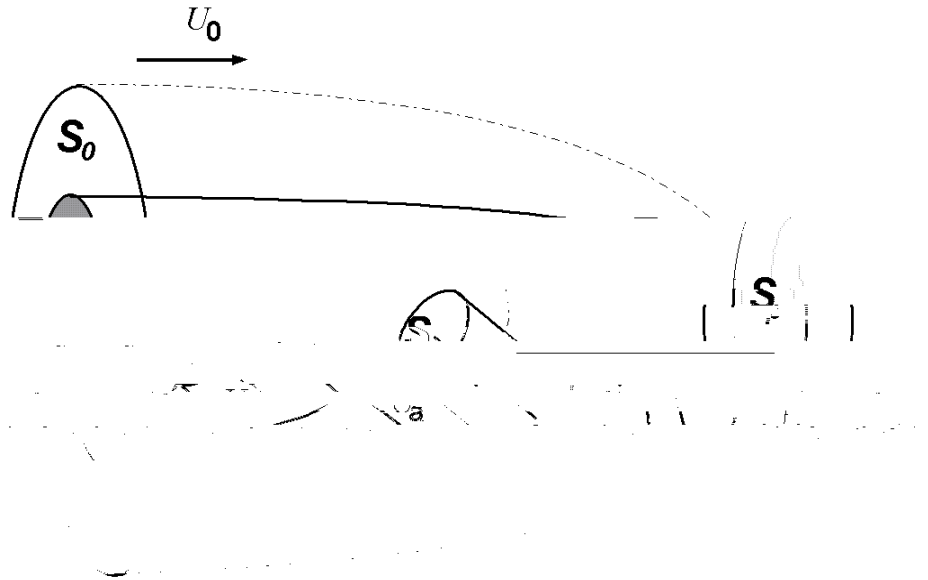
$C_0$



$$A = f(R_a, d_p, f_p, L_i, St, v_s, Re, B)$$



# Sampling in moving air



$$A(t) = \frac{N_a(t - \frac{x}{U_0})}{N_0(t)} \frac{\int_{S_a} c_a(x, y, t - \frac{x}{U_0}) v_{pa}(x, y, t - \frac{x}{U_0}) dy dx}{\int_{S_0} c_0(x, y, t) v_{p0}(x, y, t) dy dx}$$

# Lagrangian equations of particle motion

$$m \frac{d\bar{v}}{dt} = m \bar{u} \cdot \bar{v} + m \bar{A} \cdot t + m \bar{g} + \bar{F}_e$$

Aerodynamic drag

Brownian force

gravity force

electrostatic force

$$3d a d / c_s m$$

$\bar{v}$   $\bar{v}(x, y, z)$  particle velocity  
 $\bar{u}$   $\bar{u}(x, y, z)$  air velocity

$a$  viscosity

$d$  particle diameter

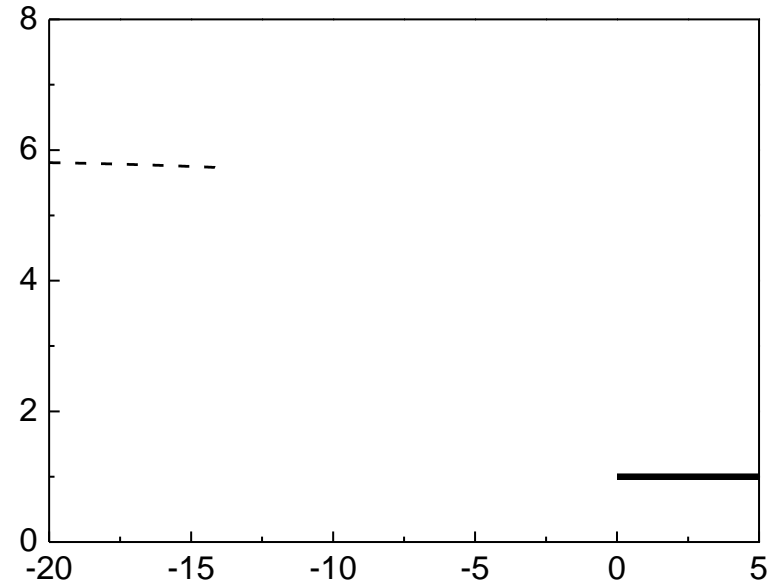
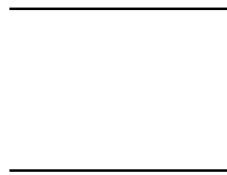
$m$  particle mass

$c_s$  Cunningham correction factor

# Thin walled sampler for very small velocities ratio

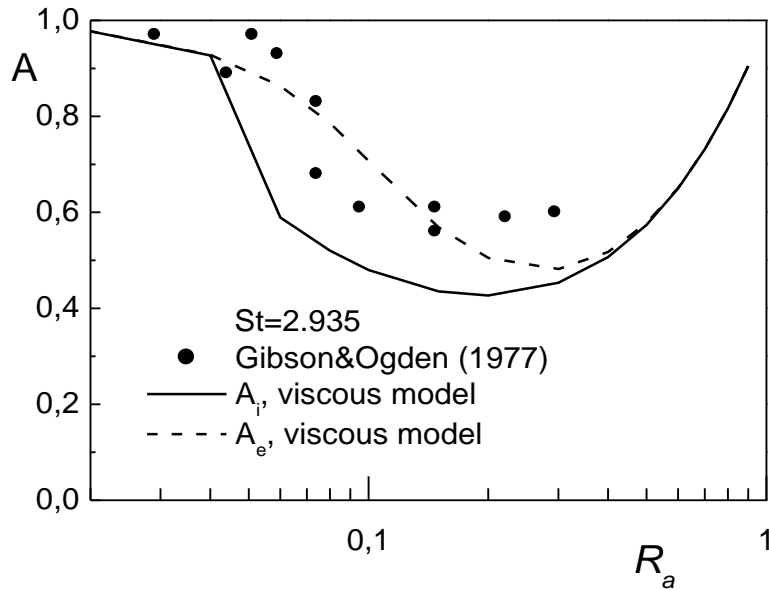
S.K. ZARIPOV, A.K. Gilfanov, D.V. Maklakov Numerical study of thin-walled sampler performance for aerosols in low windspeed environments. Aerosol Science and Technology, 2010.

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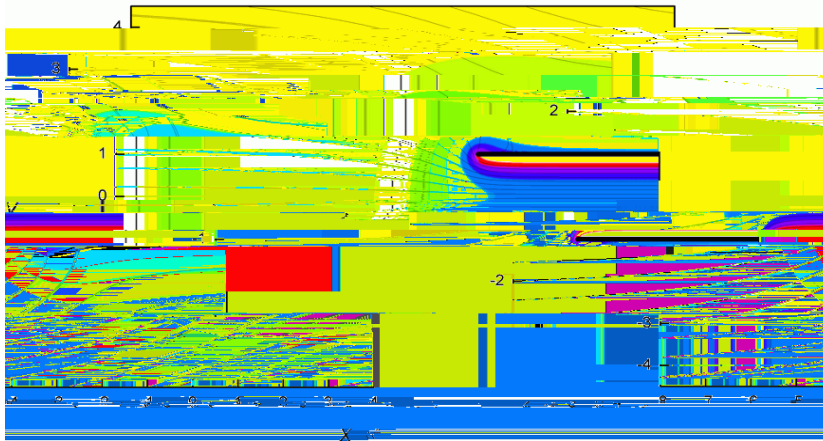
Comparison of  $A_i(Ra)$   $A_e(Ra)$  and experimental data  
Gibson&Ogden (1977) Davies&Subari (1982)

0,1

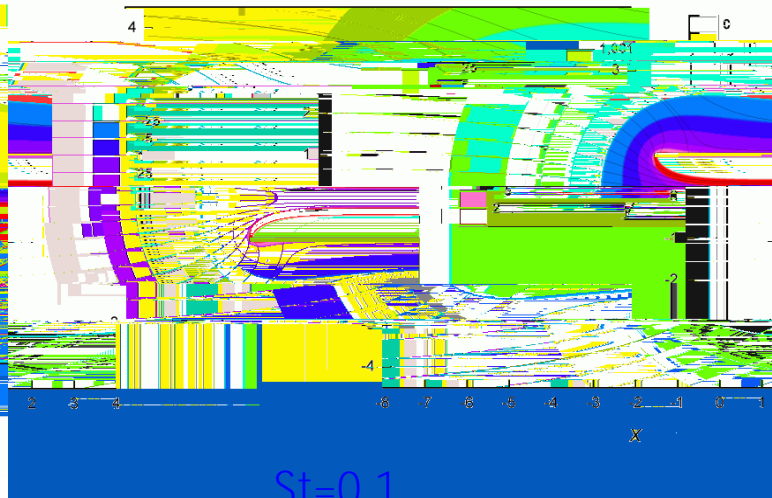




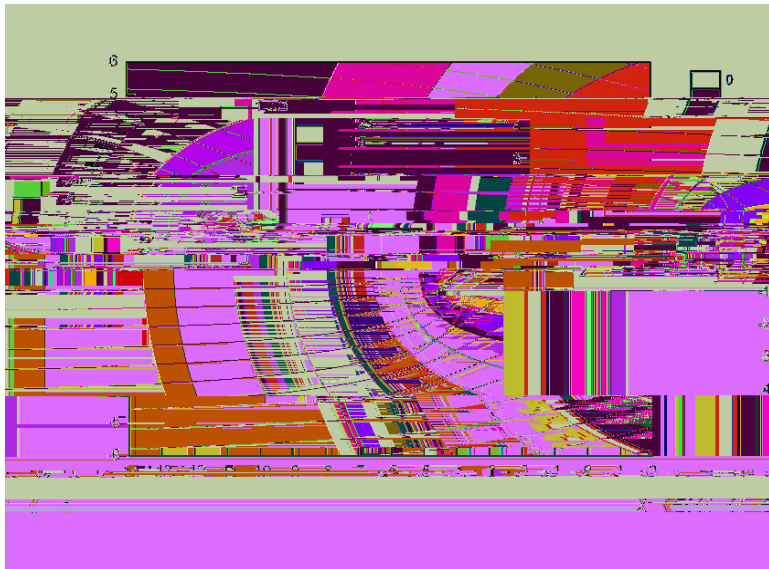
Particle concentration contours for  $a=0.2$  (lines = particle trajectories)



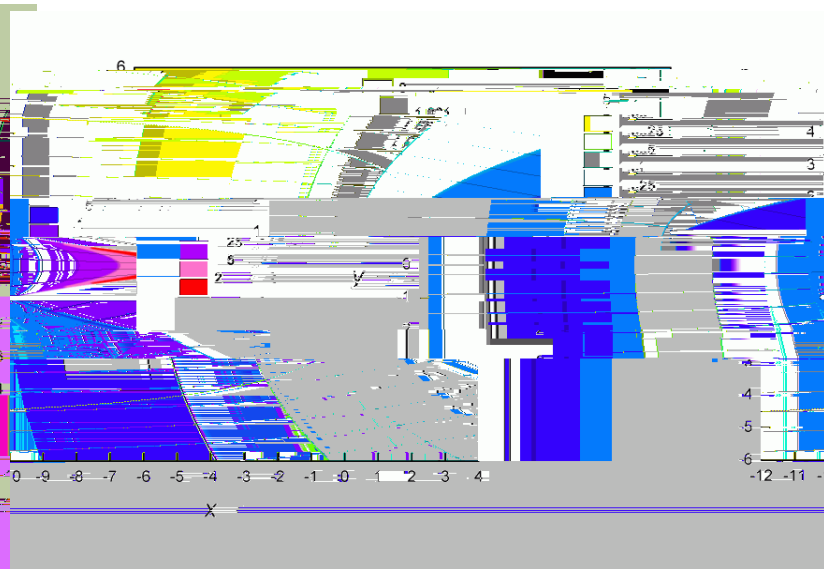
$St=0.01$



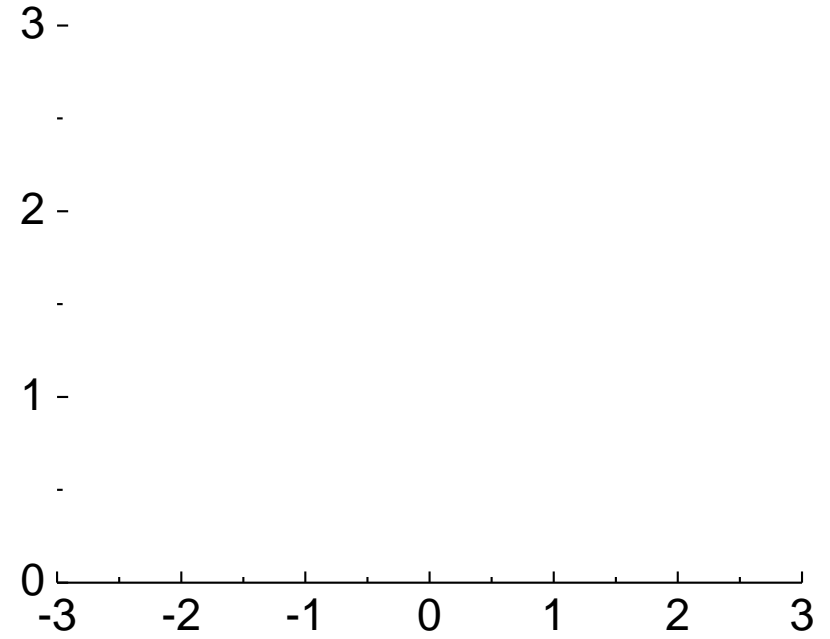
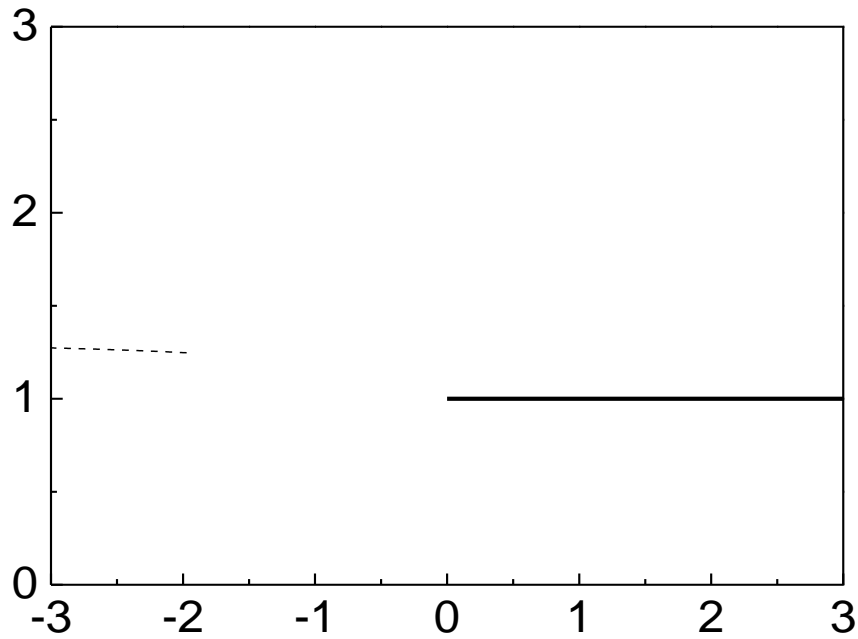
$St=0.1$



$St=1$



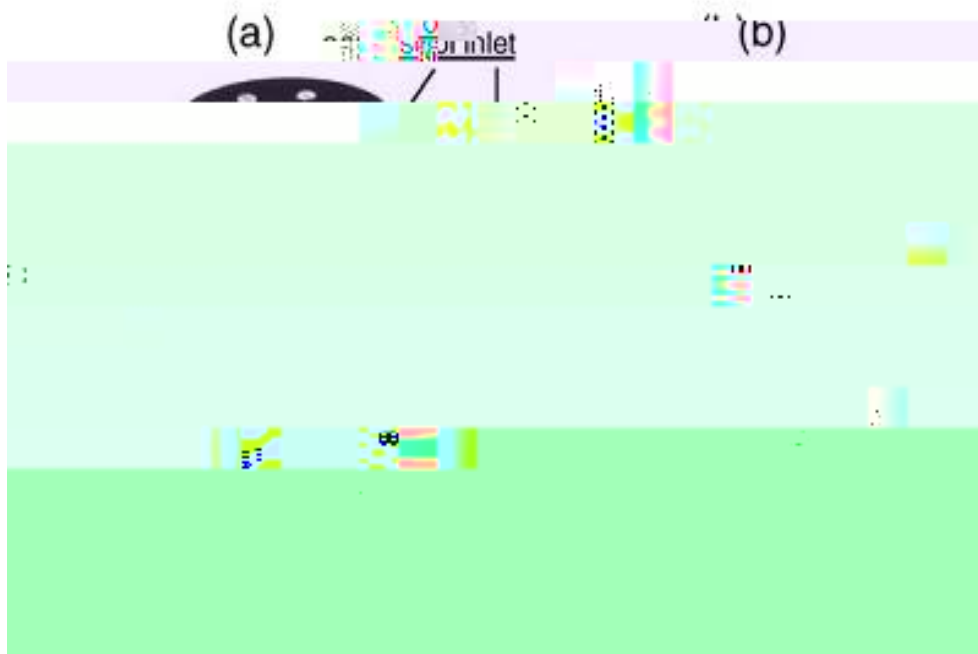
$St=10$



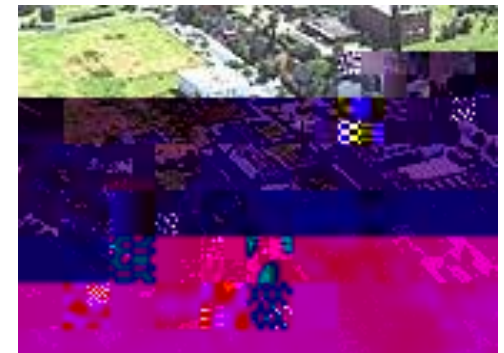
Particle trajectories and concentration isolines  
 $R_a=0.2$  and  $St=1$  for potential and viscous flows

# Numerical study of performance of the RespiCon sampler in calm air

W. Koch et.al., 2009



FRAUNHOFER INSTITUTE  
TOXIKOLOGIE UND  
EXPERIMENTELLE  
MEDIZIN, HANNOVER





# Numerical study of performance of the RespiCon sampler in calm air

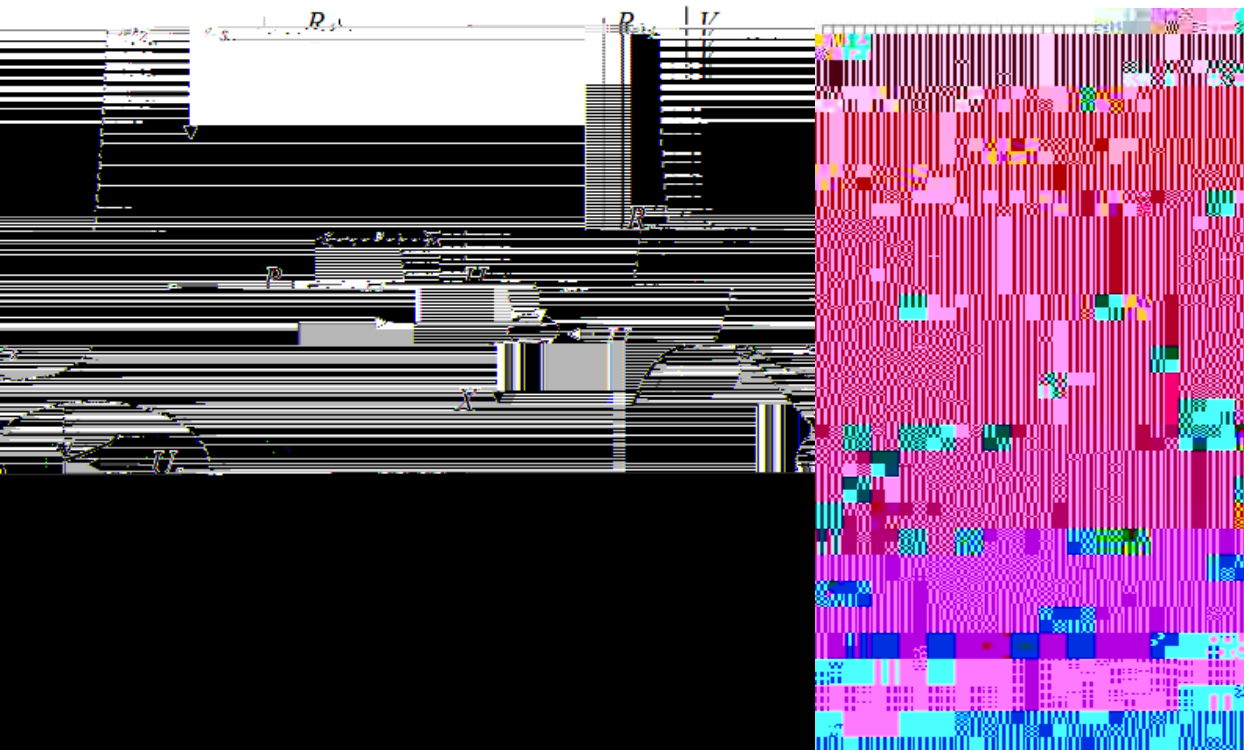


Fig. 2. RespiCon sampler scheme and mesh of calculation domain

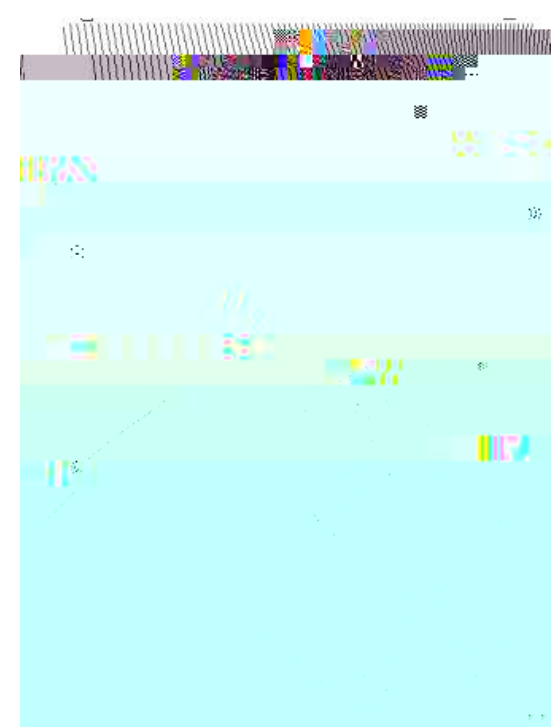
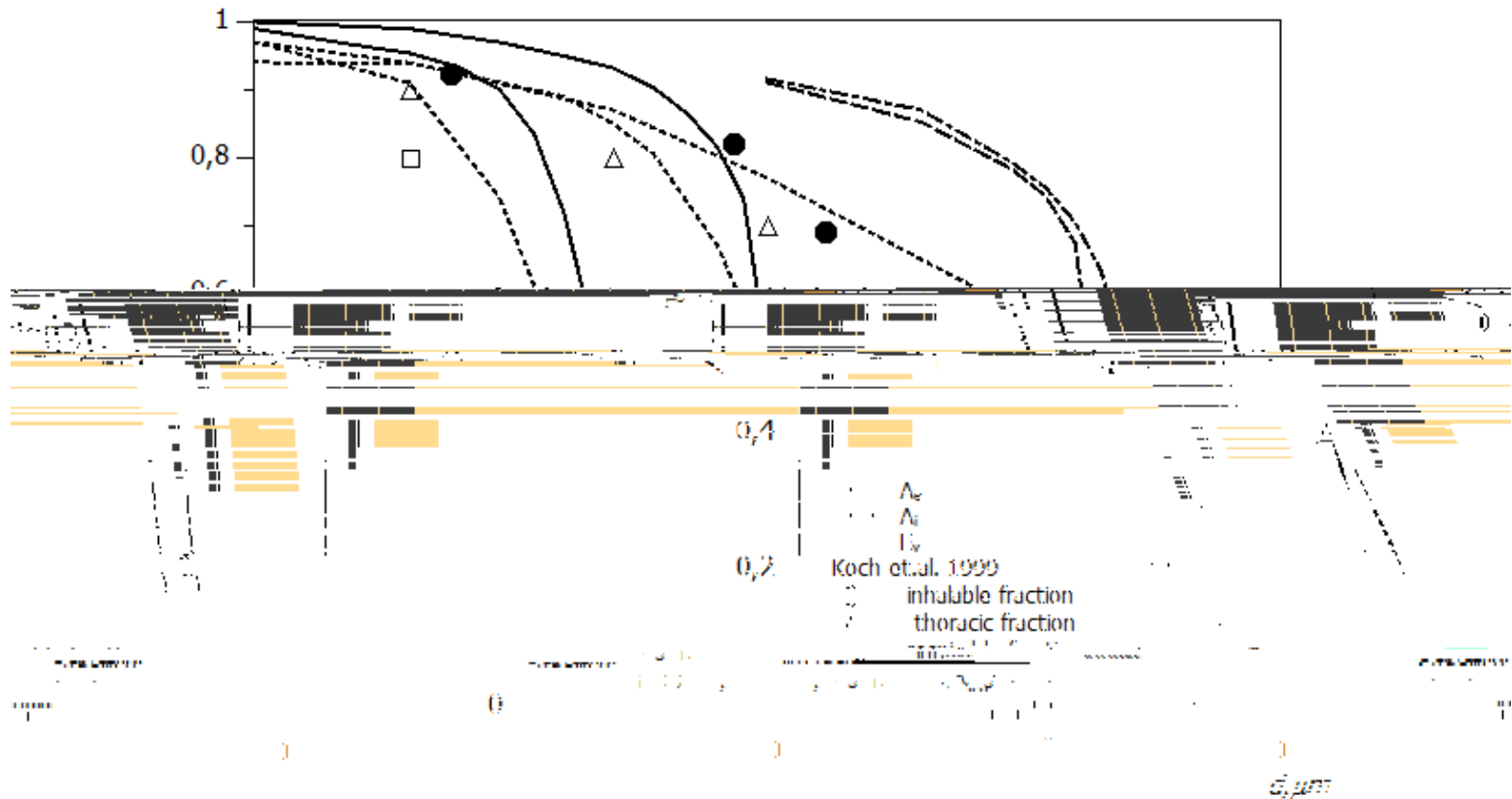


Fig. 4. Example of trajectories of particles impacting the slit wall

# Collection efficiencies of RespiCon stages as a function of particle diameter





# Sampling into spherical sampler in calm air

$$\bar{U}_0 = 0 \quad R_a = 0$$

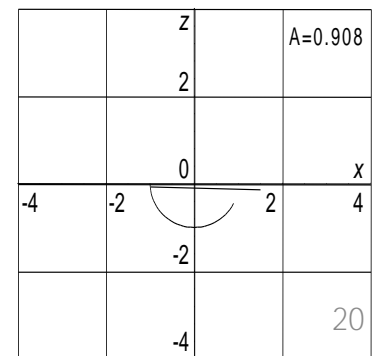
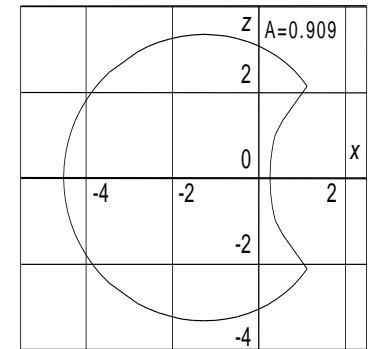
$$= 12$$



$$= 0$$

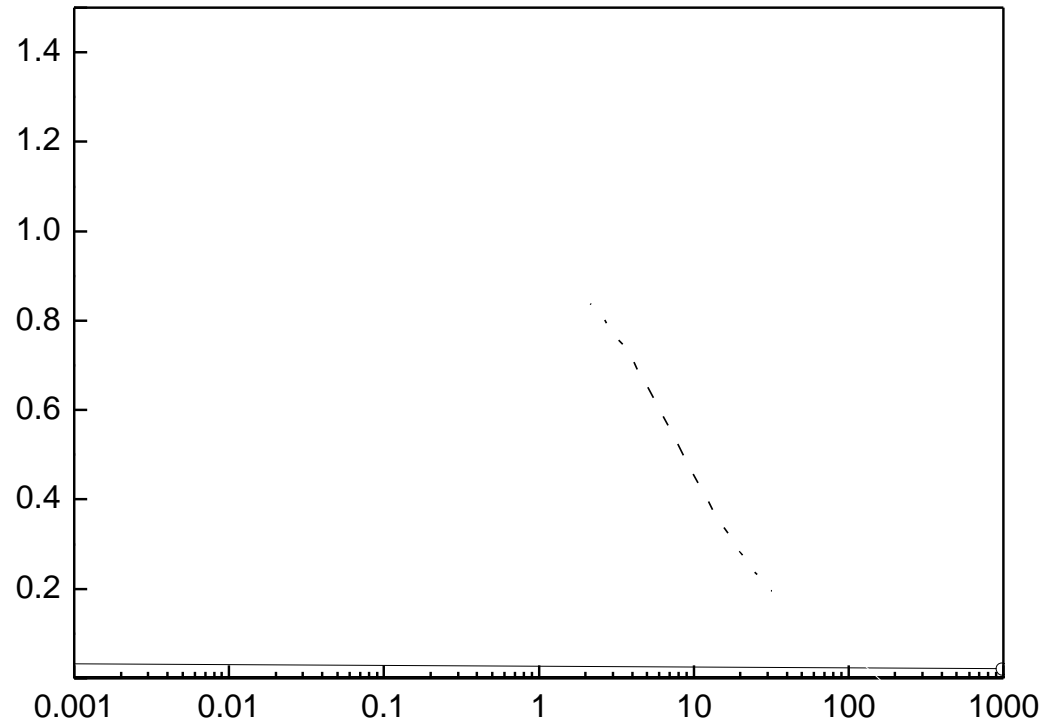
$$= 12$$

P


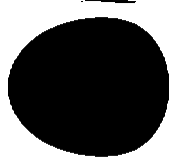


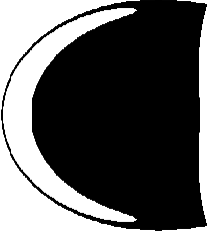
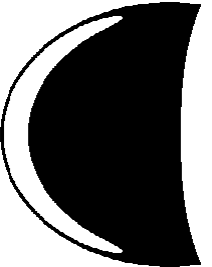


20

=d



$A(\text{St}_c)$      $V_s=0.1$      $0.01$

					
$R_a=0.15$	$R_a=0.1$	$R_a=0.075$	$R_a=0.05$	$R_a=0.025$	$R_a=0.0$

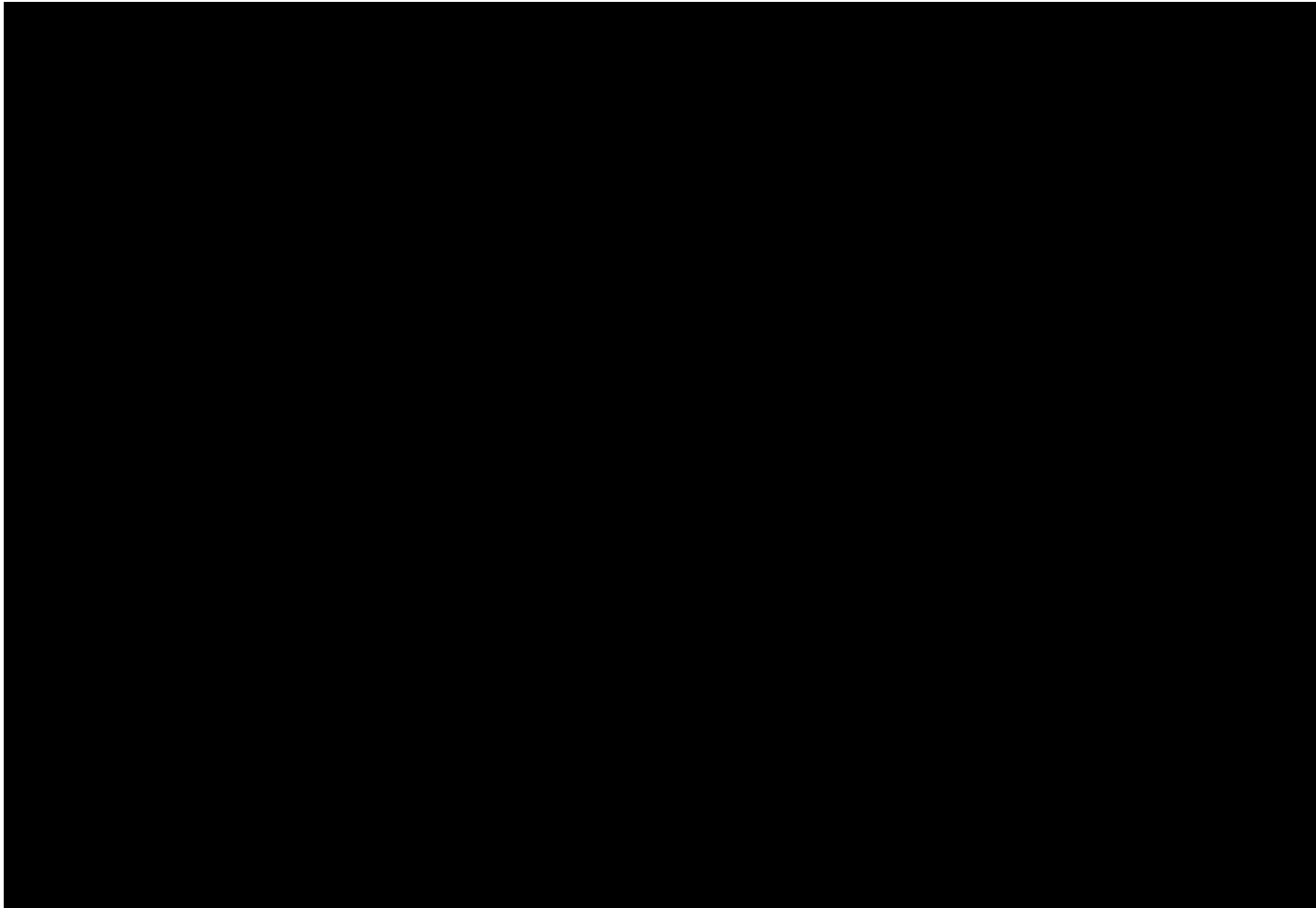
**Fig.3.**

$$A \quad 1 \quad k \quad k^2$$

$$k \quad \text{St}(R_a^2 \quad R_c^2)^{3/4} \quad 1$$

$$=-15.19, \quad =$$

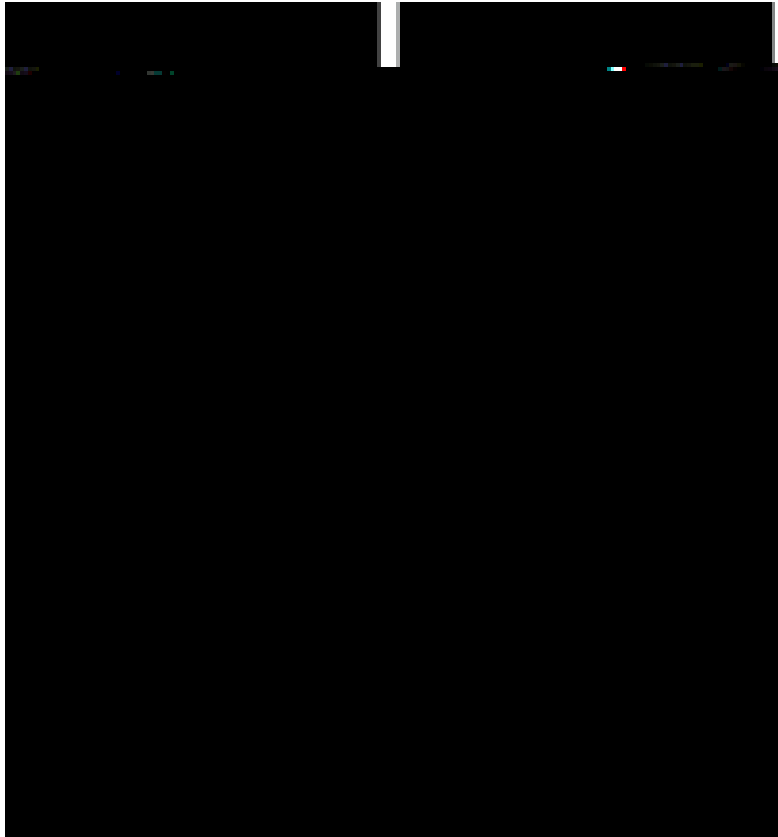
## Aspiration efficiency - Inhalation fraction



$$\text{IPM} = 0.5(1 - \exp(-0.06d_p))$$

The criterion for inhalable particulate mass (IPM) from the American Conference of Governmental Industrial Hygienists (ACGIH)



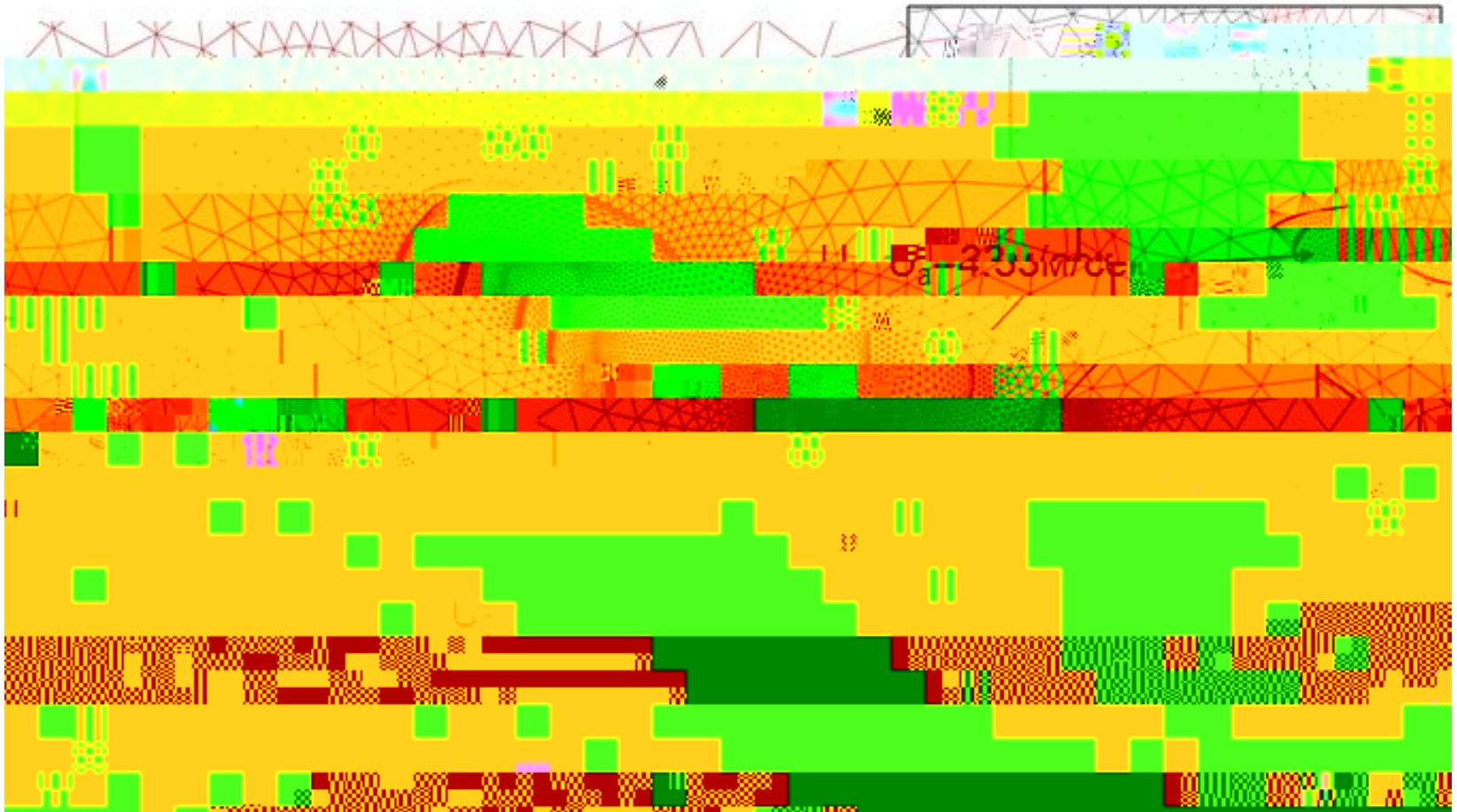


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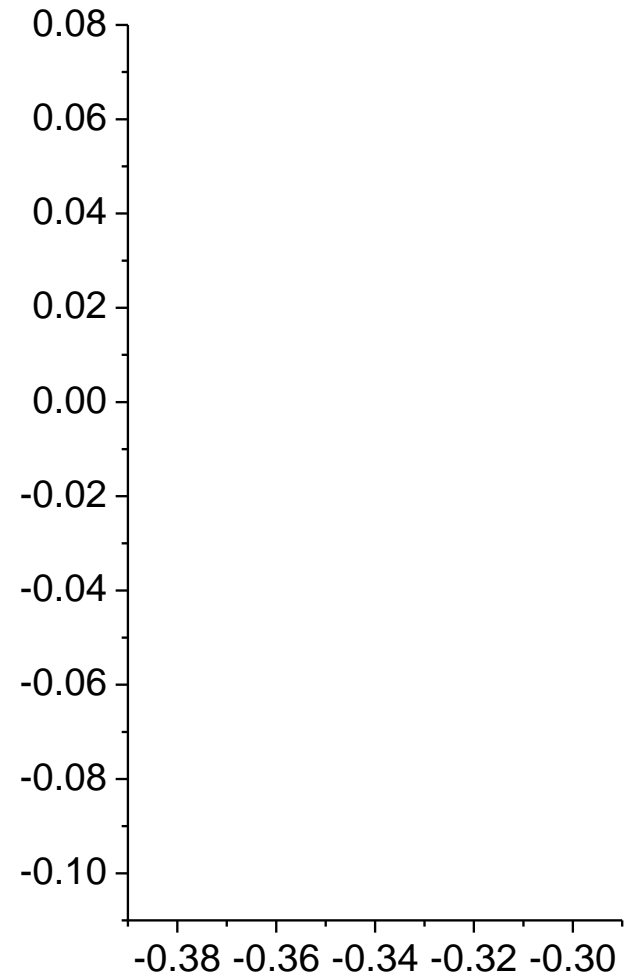
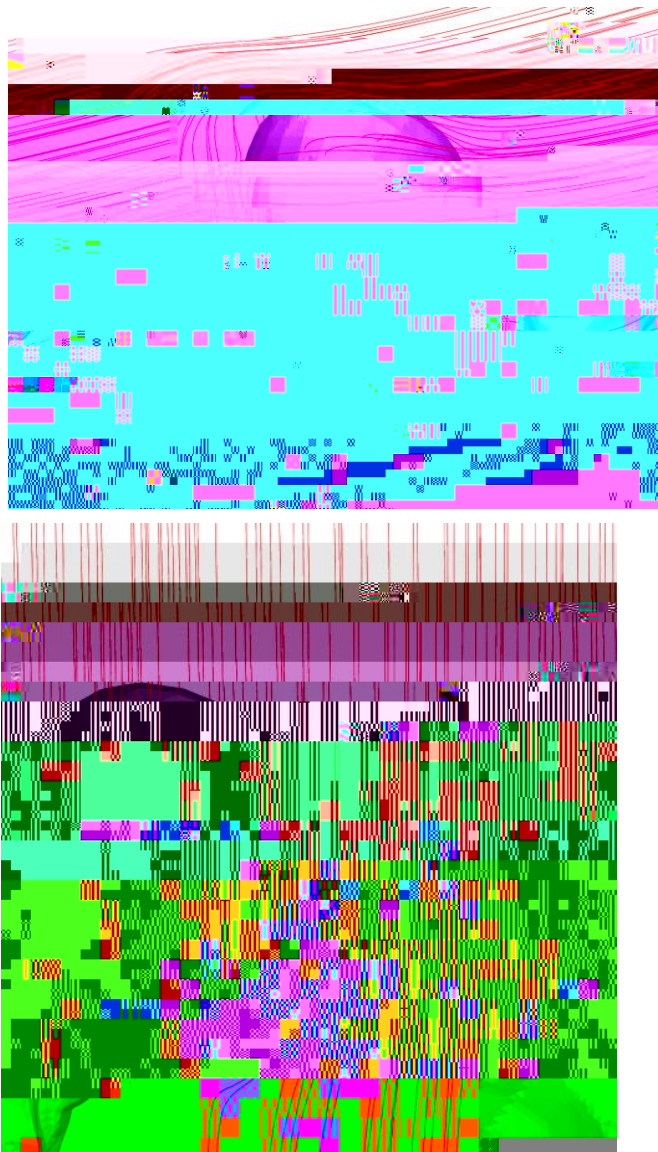
**Experimental methods to determine inhalability and personal sampler performance for aerosols in ultra-low windspeed environments**

*J. Environ. Monit.*, 2008

# CFD model of aerosol flow in the vicinity of manikin head



Meshing in the vicinity of manikin head



The trajectories of particles at  $d=37\mu\text{m}$  for two wind velocities: a- $U_0=0.2$  m/s, b -  $U_0=0$

The area  $S_p$  of the aspirated particles

**Inhalable fraction for breathing through mouth (1) and nose (2) in calm air**

# Facepiece filtering respirators (FFR) and surgical masks

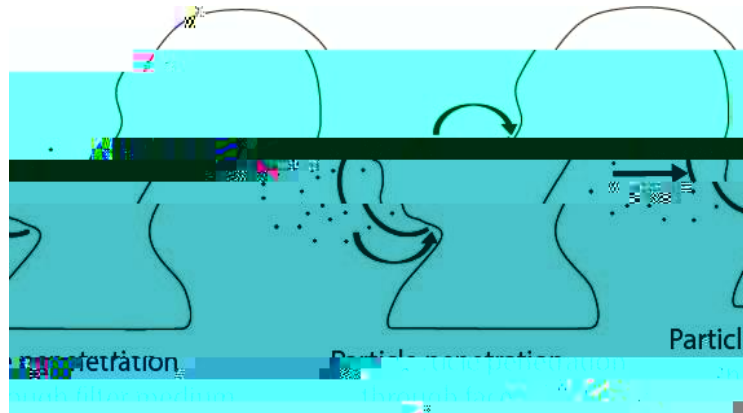
## Variety of respirator facepieces



## Performance evaluation on a manikin headform



## Two pathways of particle penetration



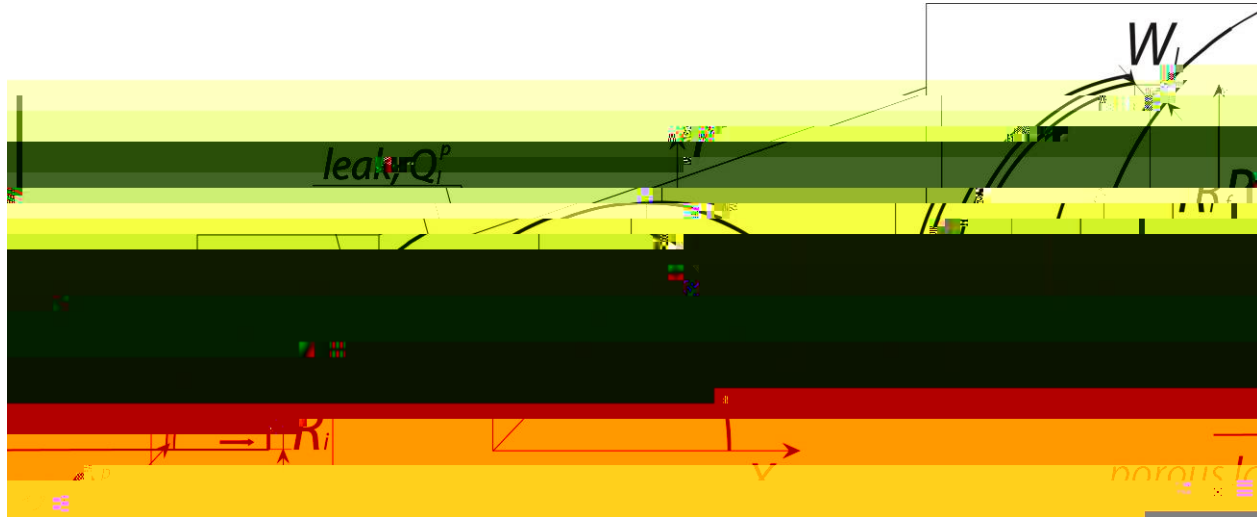
$$\text{Protection factor} = C_{\text{out}}/C_{\text{in}}$$
$$\text{Particle penetration} = C_{\text{in}}/C_{\text{out}}$$

Experimental (combining manikin-based and human study protocols):  
**Grinshpun et al. (2009).**

Leak flux / Filter flux

Particle diameter (  $\mu\text{m}$  )

# An



# Penetration of aerosol particles through filter layer

$$I_f = \exp\left(-\frac{4 E_f L}{d_f (1 - \epsilon_f)}\right)$$



# Fitting the porous layer permeability to the experimental curves $f(d_p)$ from Rengasamy and Eimer (2012)

Kozeny-Carman formula:

$$k = \frac{\gamma^3 d_{fiber}^2}{180(1 - \gamma)^2}$$

Permeability used for calculations:

$$k = 9.55 \cdot 10^{-11} \text{ m}^2$$

---

The particle penetration through the filter  $f(d_p)$  at  $Q_i = 30 \text{ l min}^{-1}$

- 1 approximated formulas  $d_{fiber} = 0.069$ ,  $L = 3 \text{ mm}$
- 2 experimental values from Rengasamy and Eimer (2012).

# Parameters and conditions used in the modeling

$$R_i = 0.007 \text{ m} \quad (S_i = 0.000154 \text{ m}^2)$$

$$R_h = 0.09 \text{ m}$$

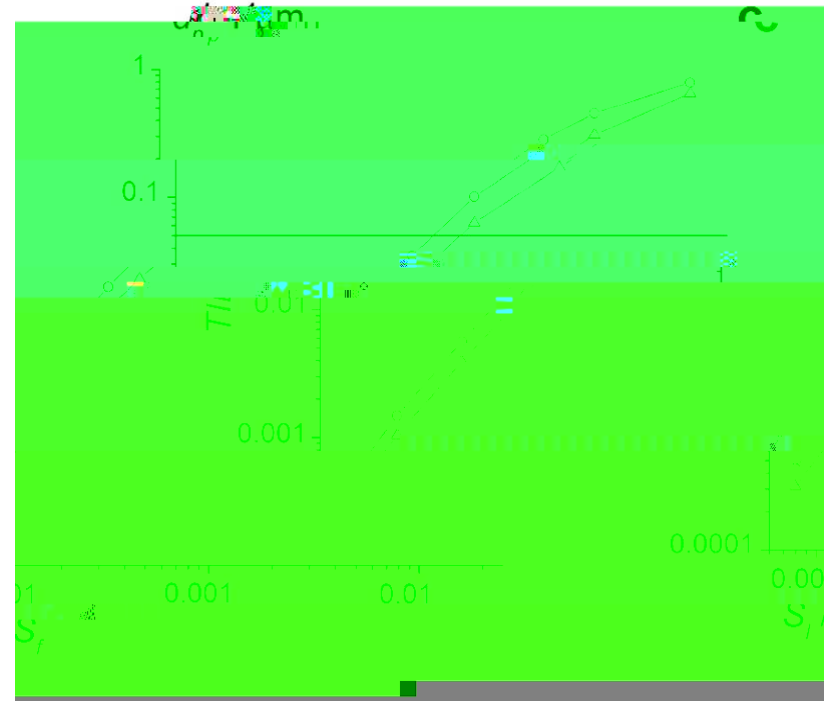
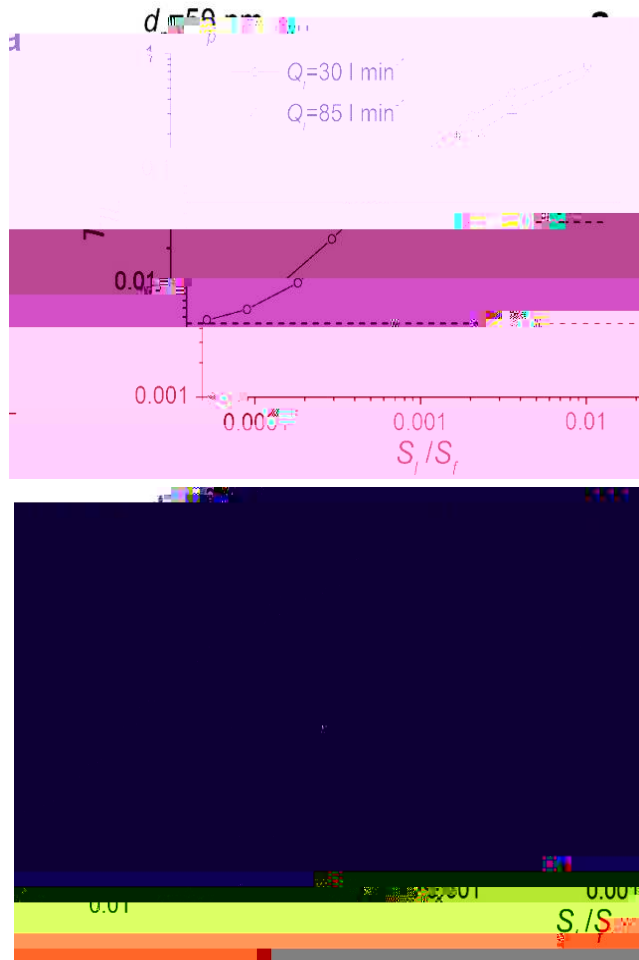
spherical segment with  
a height of  $H$

# Comparison to the experimental data of Rengasamy and Eimer (2012)



## MODELING RESULTS:

$TIL = f(S_l/S_f)$  at  $d_p = 50$  nm (a), 100 nm (b), and 1  $\mu\text{m}$  (c)  
for different inhalation flow rates

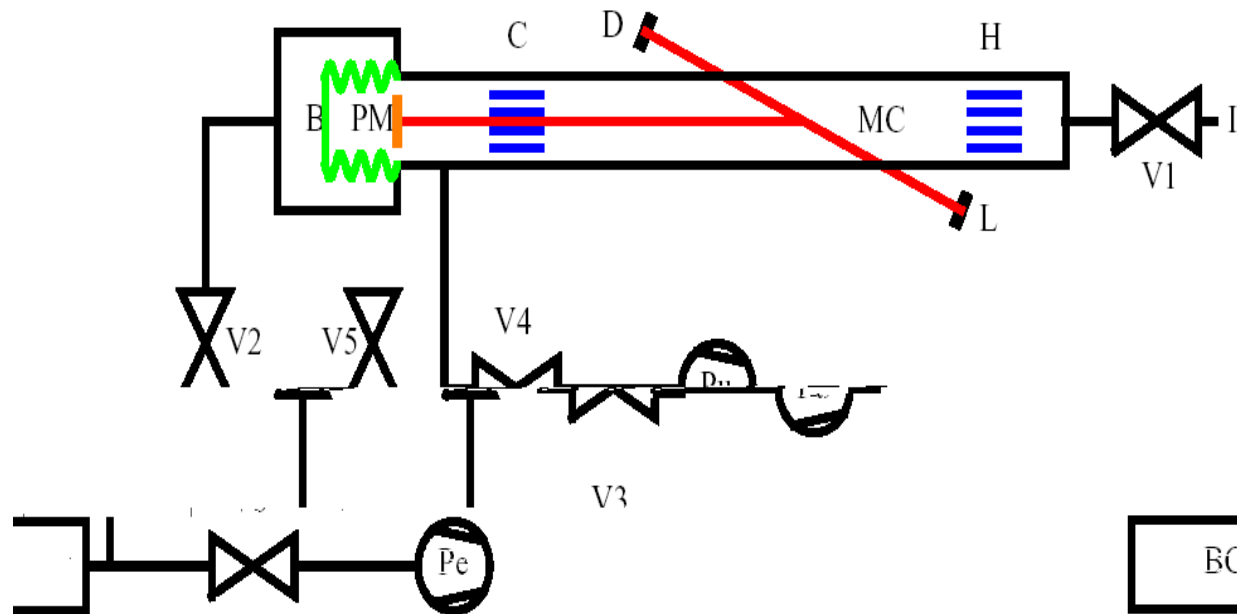


Solid lines represent the target value for an N95 ( $TIL=0.05$ ).

Dotted lines represent a "perfect fit" respirator (with no faceseal leakage).

# NUMERICAL STUDY OF GROWING DROPLETS DYNAMICS IN UNSTEADY THERMAL CONVECTION FLOW

S.K. ZARIPOV , R.S.Galeev , W.Holländer. Numerical study of dynamics of growing droplets in Kelvin spectrometer. Abstracts of European Aerosol Conference-2007, Salzburg, T12A033.

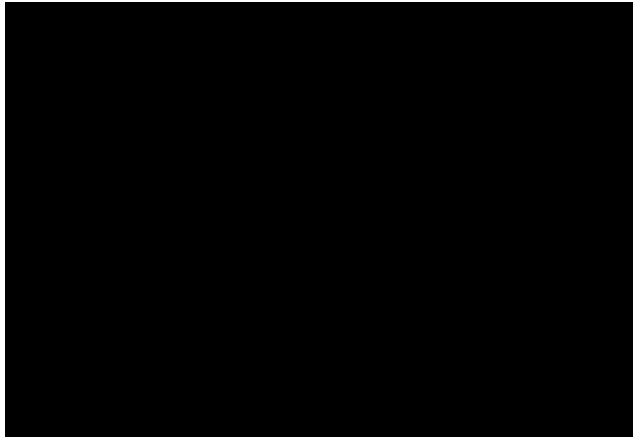


The main channel is equipped with a pump (Pe) and a valve (V2). The flow is controlled by valves V3, V4, and V5. The pressure is measured by a gauge (Pe). The chamber (C) is equipped with a motor (PM) and a valve (V1). The chamber (MC) is equipped with a motor (PM) and a valve (V1). The chamber (H) is equipped with a motor (PM) and a valve (V1). The chamber (BC) is equipped with a motor (PM) and a valve (V1).

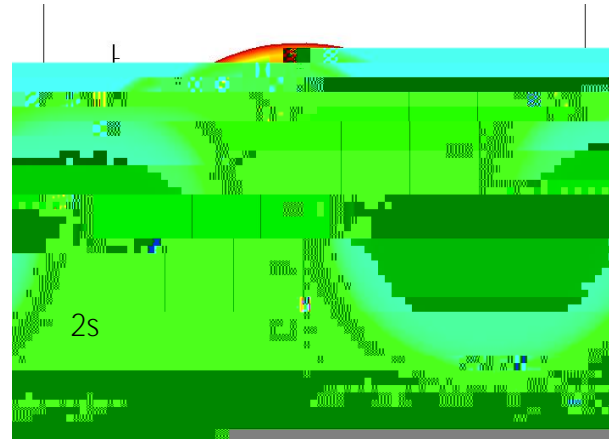
Fig.8. Time evolution of the temperature distribution in the cross section of the horizontal cylinder

$$T_w(\bar{r}_p, t)$$

1s

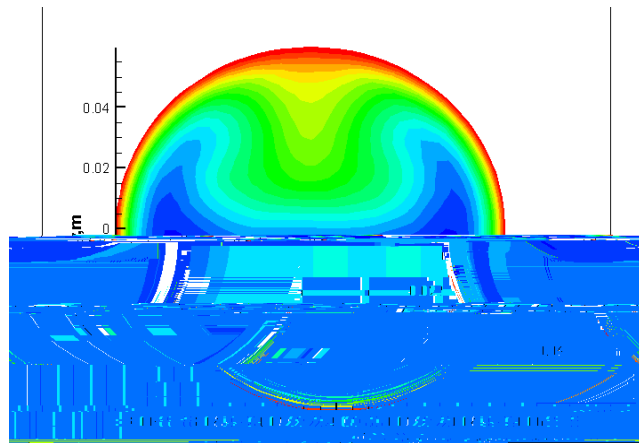


2s

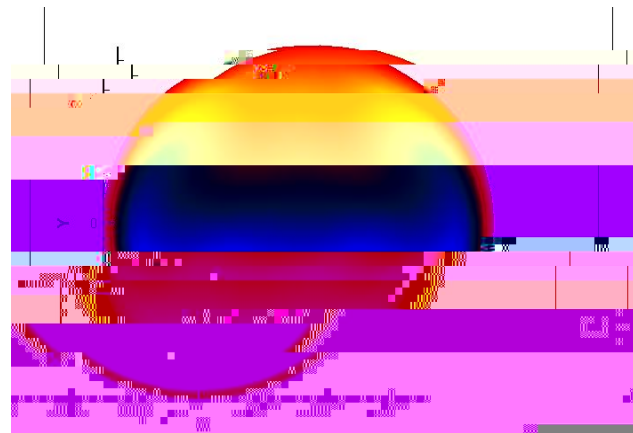


2s

5s

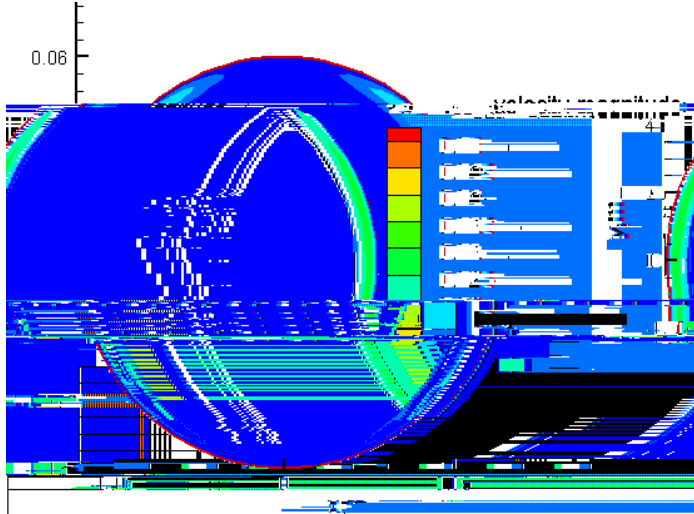


10s

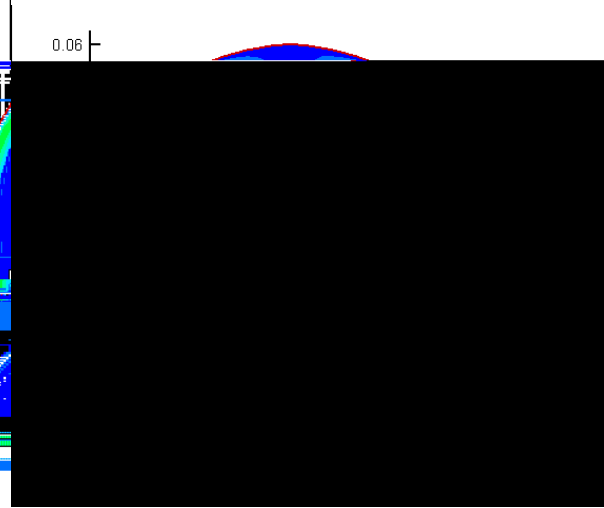


$$\bar{U}(\bar{r}_p, t)$$

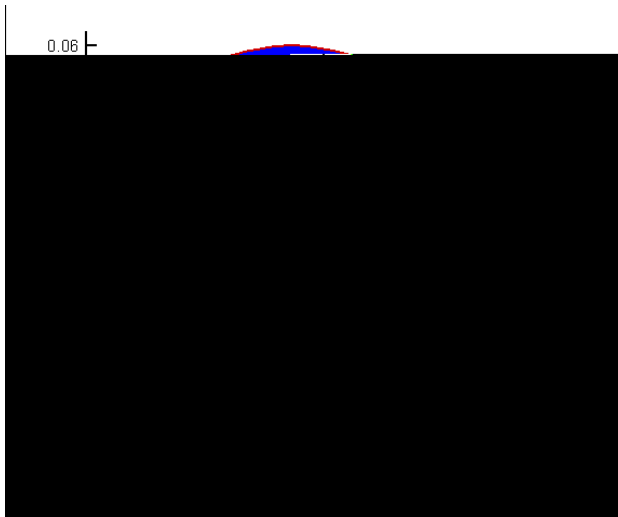
1s



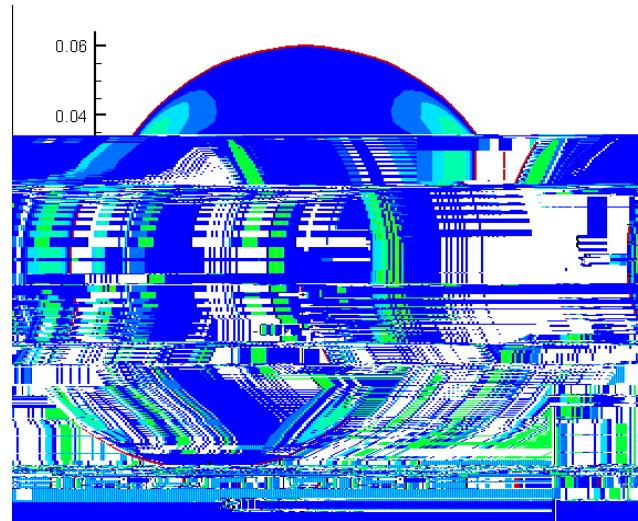
2s



5s



10s



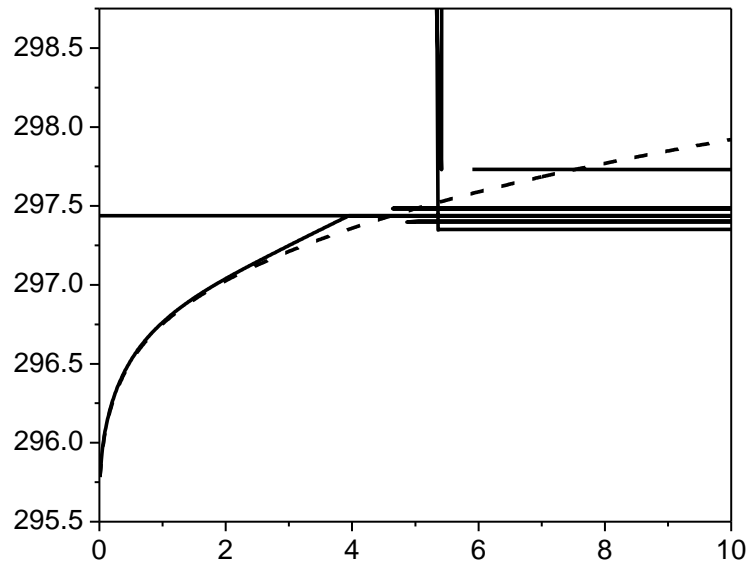


Fig.7. Average gas temperature with and without convection influence

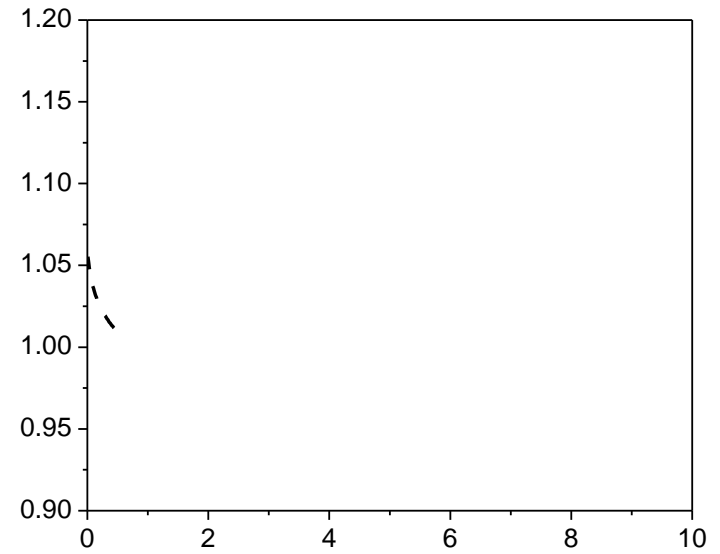


Fig.8. The saturation based on the average temperature gas temperature with and without convection influence



# 2019年1-9月中国主要农产品进口情况

数据来源：海关总署

单位：亿美元



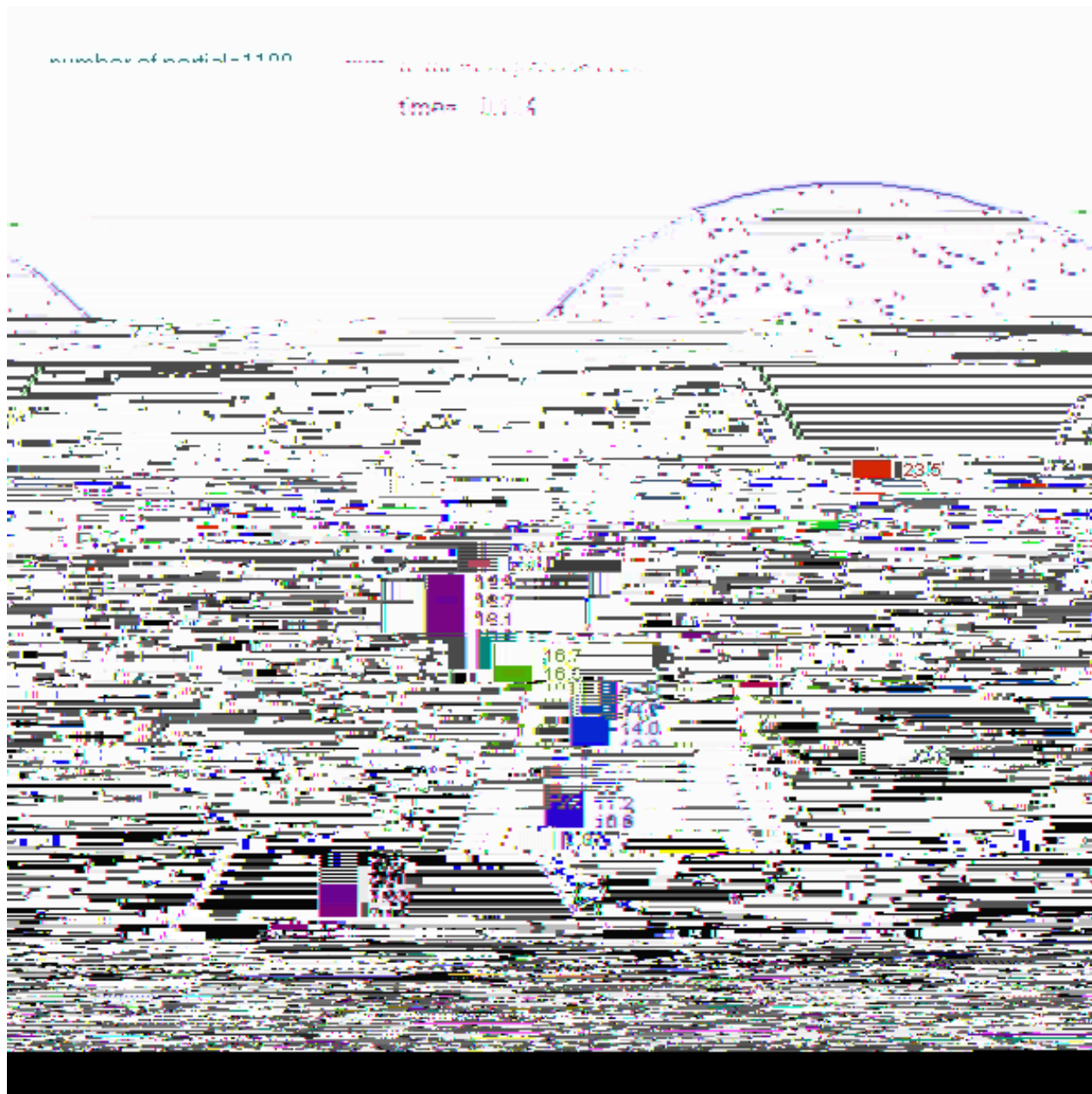
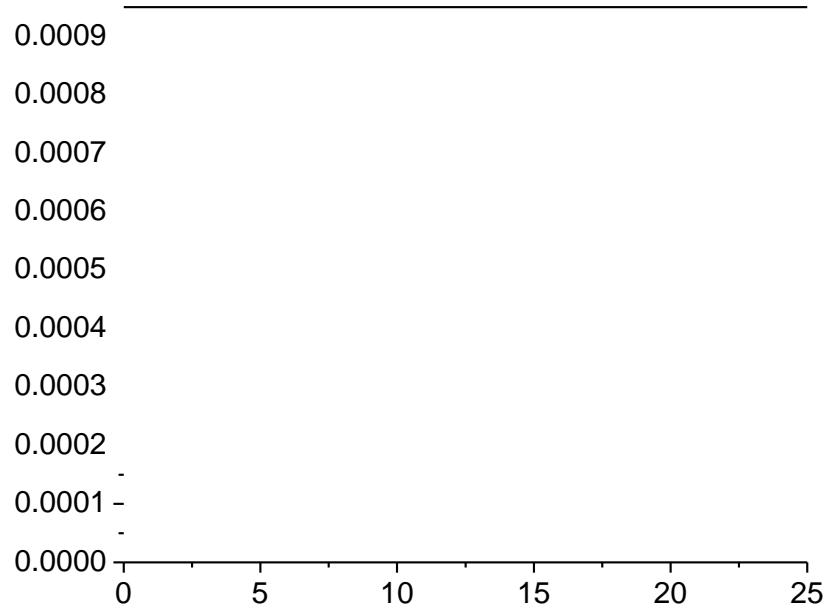
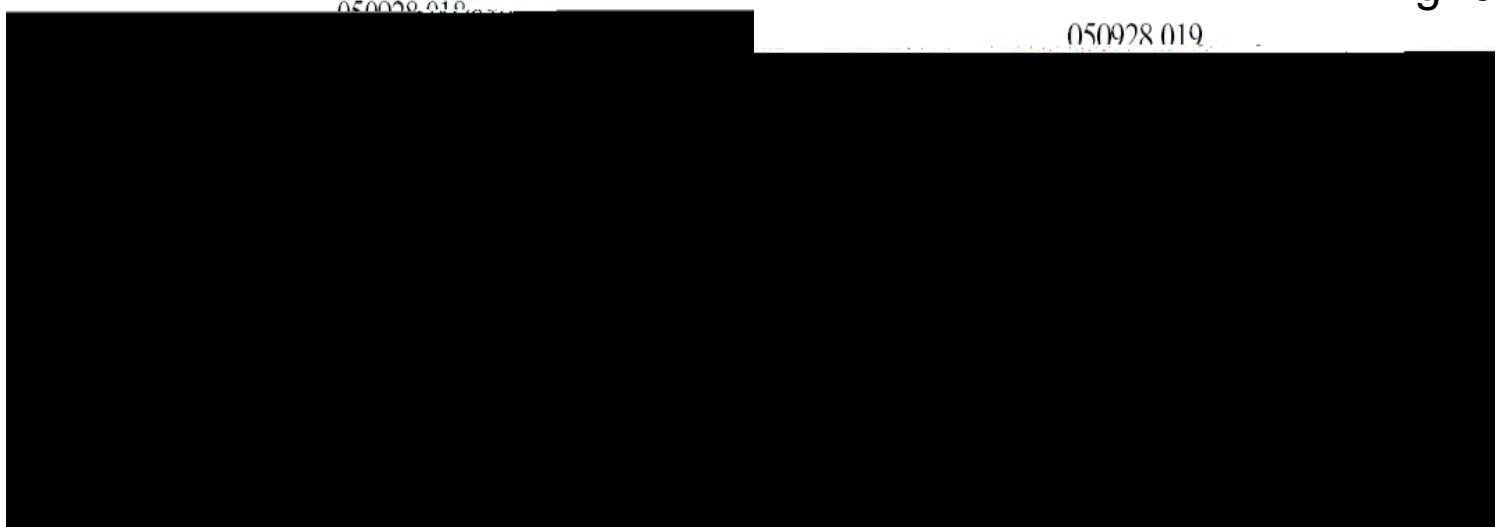


Fig.14. The mass density of condensing vapor on all droplets for  $N=1000 \text{ cm}^{-3}$  and various initial saturations



$g=9.81\text{m/s}$

$g=0$



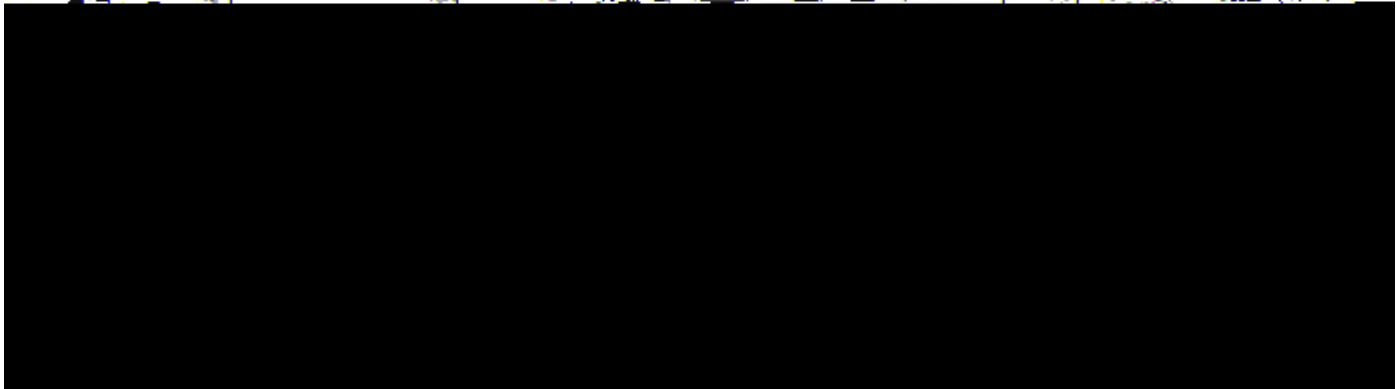
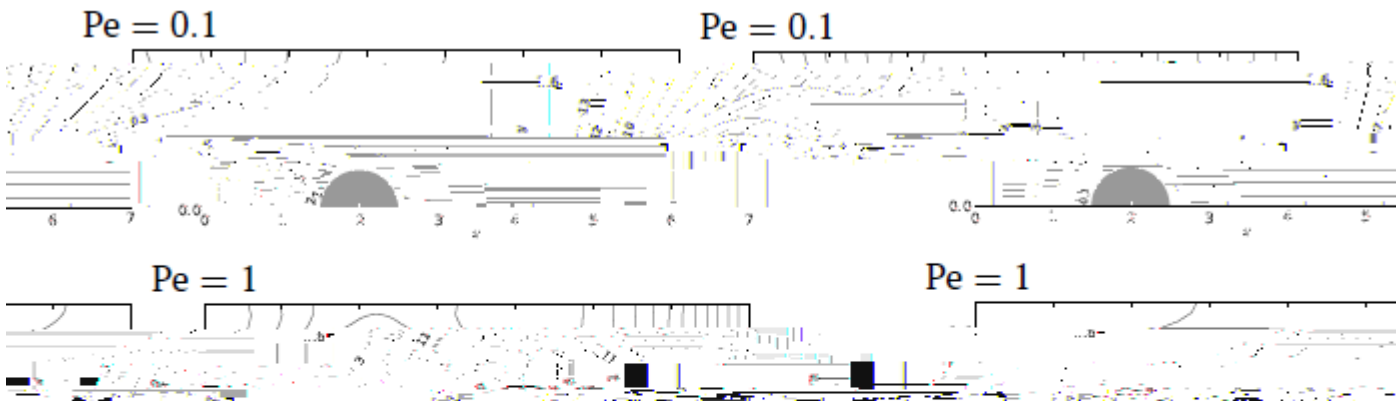
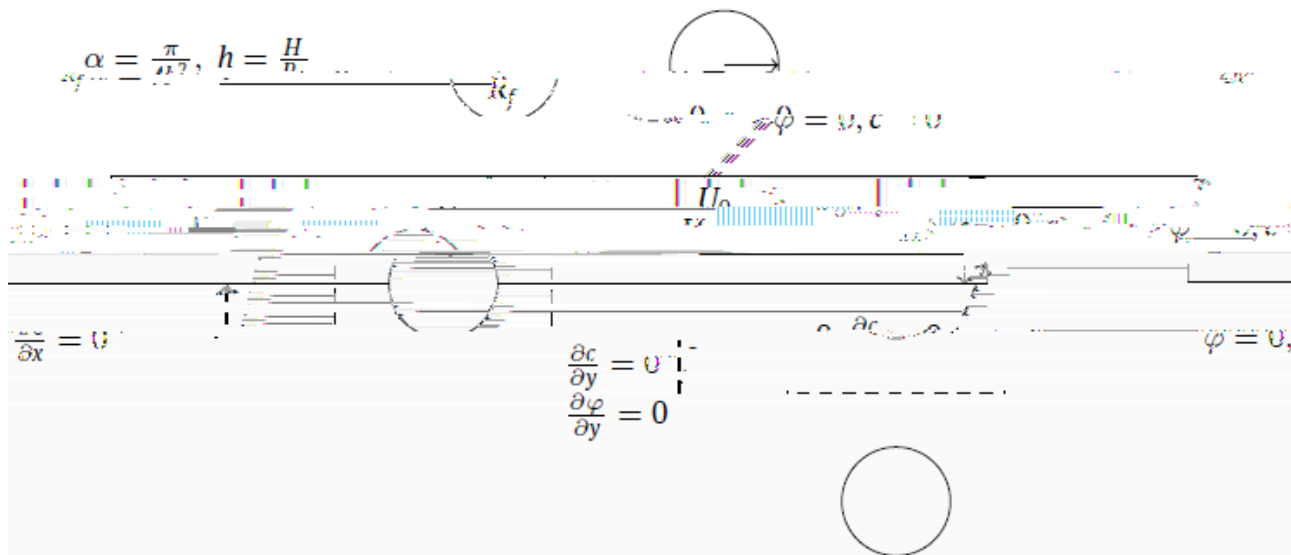
## Transport equation

$C(\bar{r}, t)$  - particle concentration

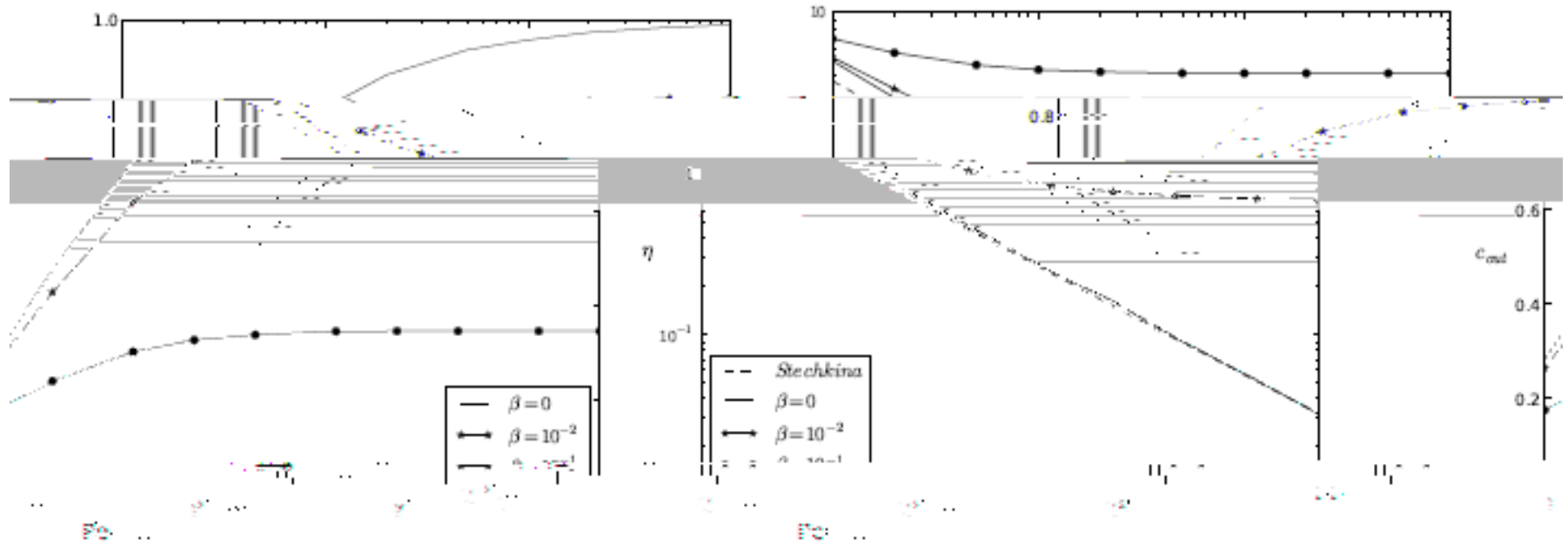
$J_D = -D \nabla^2 C$  Diffusion flux

$J_u = C \bar{U}$  convective transport

$$\frac{\partial C}{\partial t} = D \nabla^2 C - \bar{U} \cdot \nabla C + \text{sources/sinks}$$



# Deposition efficiency



# Aerosol deposition on the porous cylinder

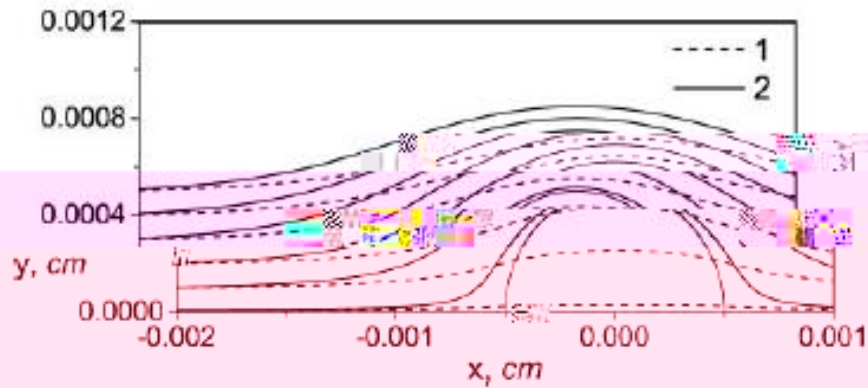
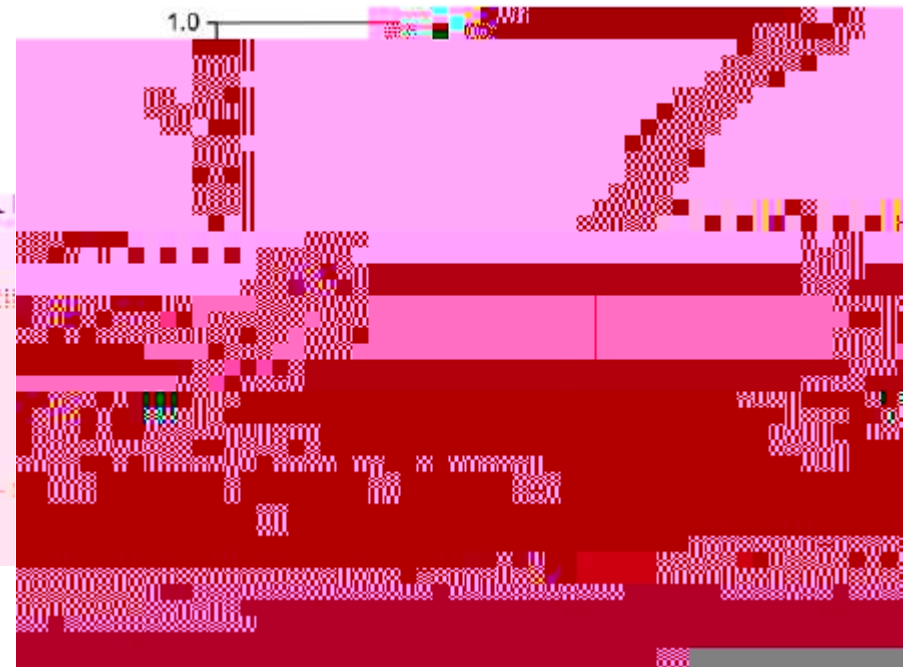


FIG. 4. Streamlines from numerical model  $\alpha=0.05$ : (1)  $Da = 10^{-2}$ , (2)  $Da = 10^{-3}$ .





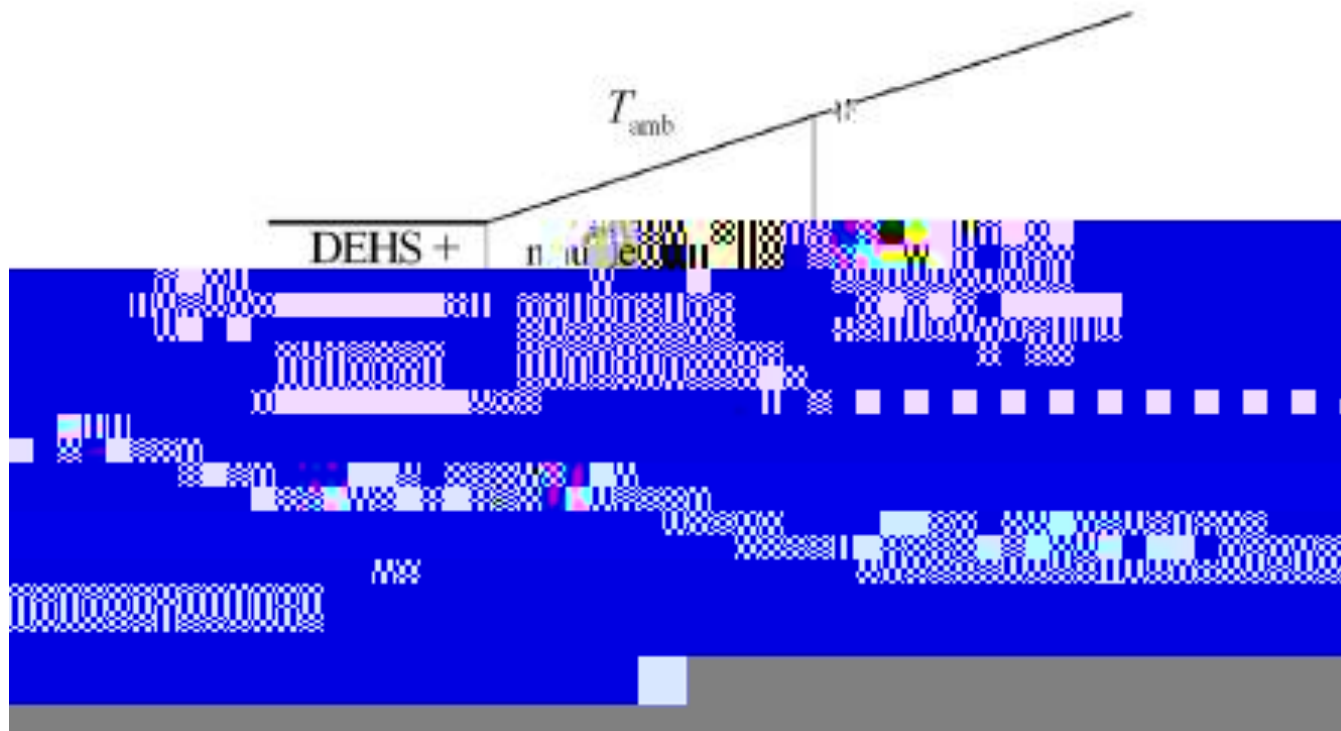








A.K. Gilfanov, W. Koch, S.K. Zaripov Mathematical modeling of di-ethyl-hexyl-sebacate nanoparticle formation in a free turbulent jet under high nucleation rate conditions. Journal of Aerosol Science. - 2016. - V.96. - P.124-139.



# Collaboration

## Brighton University - Kazan University

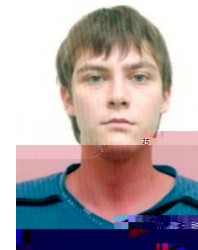
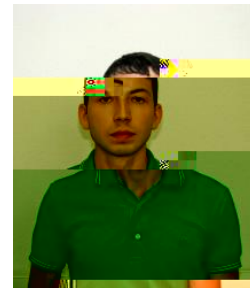
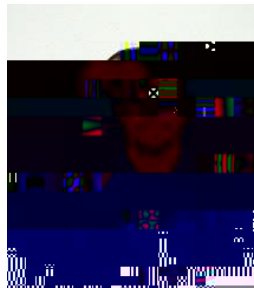
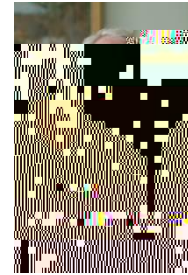
### 2016-2018

Joint project Royal Society (UK) RFBR (Russian Federation)

Modelling of aerosols/sprays for medical and  
automotive applications

## Aerosol laboratory

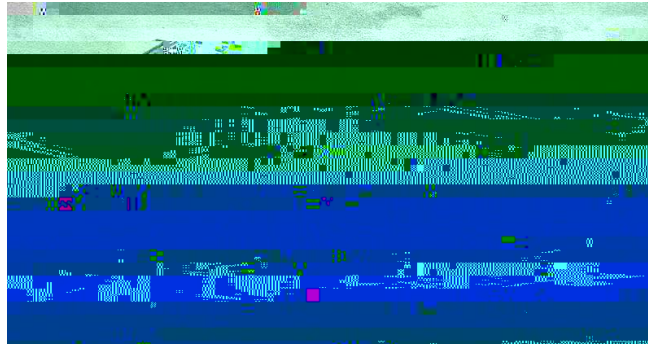
- Head Prof. Shamil Zaripov, GAeF member



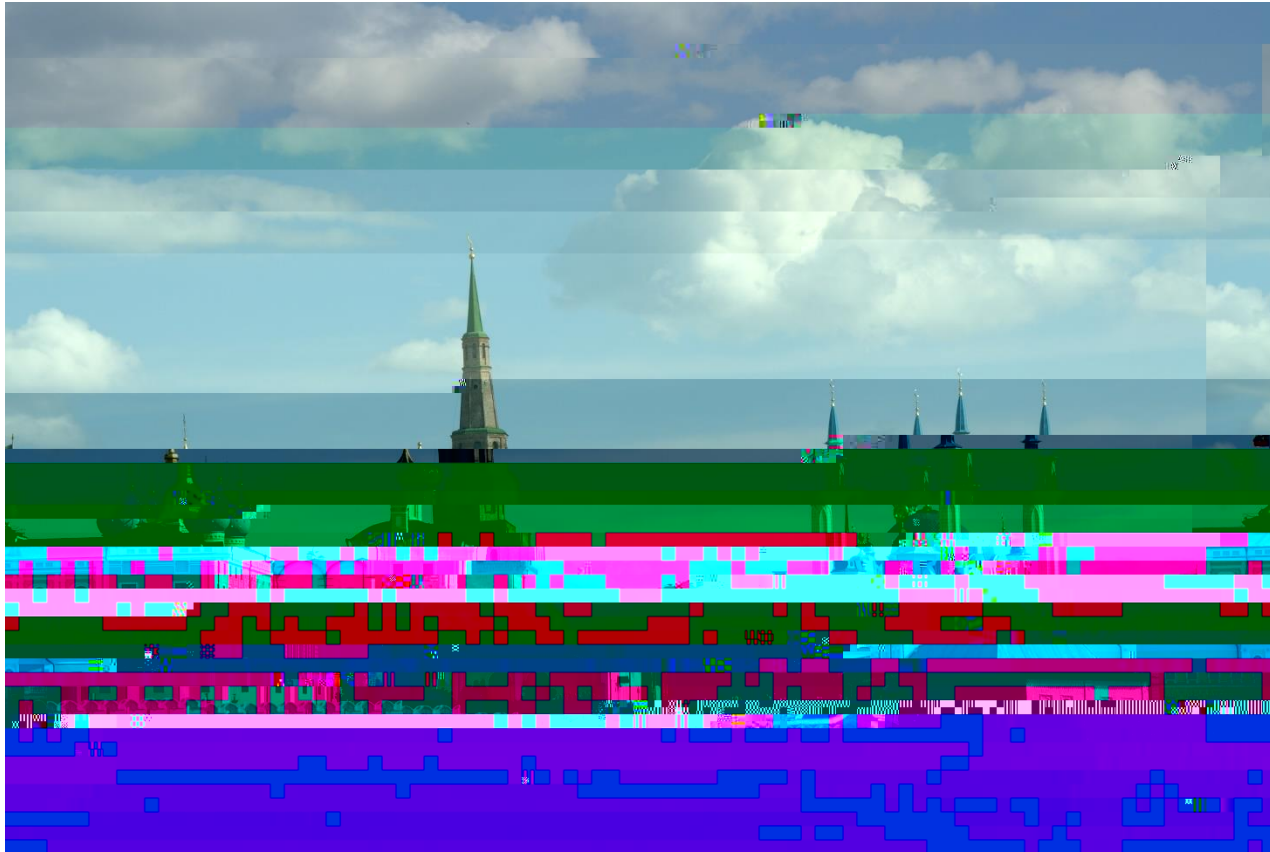
Founded in **1804**, Kazan University is the second oldest university in the Russian Federation, and now is an internationally acknowledged center of academic excellence.



Before 1878 Kazan University was the farthest Eastern university of the Russian Empire: its academic district included the Volga Region, Kama Region, Ural Region, Siberia and Caucasus.



The main center of higher education for a vast region, KFU has over 47,000 students, who follow 310 major degree programs.



Thank you for attention